

Report

Thickener Area Mini-HAZOP Report

H354600-3310-142-066-0001

2021-06-29	A1	Approved for Use	J. Yesberg	B. Stewart	P. Pouliot	S. Somasundaram
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Table of Contents

1. Executive Summary	1
2. HAZOP Scope & Methodology.....	1
2.1 HAZOP Scope	1
2.2 HAZOP Objective	1
2.3 HAZOP Methodology	2
3. HAZOP Participants	3
4. Recommendations	5
5. References.....	7

List of Tables

Table 2-1: Nodes for HAZOP Study	1
Table 2-2: HAZOP Guidewords	2
Table 3-1: HAZOP Participants.....	4

List of Appendices

Appendix A

Marked up Nodes (P&ID)

Appendix B

Mini-HAZOP Study Worksheet

1. Executive Summary

A Mini Hazard and Operability Study (HAZOP) Study was conducted for the thickener area for Project Lucy 2.0 Phase 1 on 10 September 2020. The HAZOP record is provided in Appendix C.

2. HAZOP Scope & Methodology

2.1 HAZOP Scope

The Mini HAZOP was to address design changes related to the two thickeners relocated from the DWP2 area for the first phase of Lucy 2.0. Table 2-1 shows the nodes that were to be considered. During the workshop, it was decided that there was insufficient clarity around the fire water requirement, and therefore Node 9 was not analysed.

Table 2-1: Nodes for HAZOP Study

Node	Description	P&ID
1	Thickener overflow to screen spray wash.	H354600-3300-270-276-0001 H354600-3300-270-276-0017 H354600-3300-270-276-0041
2	Screen bypass to thickener feed boxes	H354600-3300-270-276-0001 H354600-3300-270-276-0002
3	Thickener underflow to southern slurry pipeline tie-in	H354600-3300-270-276-0001 H354600-3300-270-276-0002
4	Removal of runoff water line to thickener overflow tanks	H354600-3300-270-276-0017
5	Thickener overflow diversion to KO2	H354600-3300-270-276-0017
6	Flocculant make-up water source	H354600-3300-270-276-0020
7	Thickener process water tank	H354600-3300-270-276-0040
8	Thickener air compressor	H354600-3300-270-276-0033
9	Fire Water (<i>analysis not conducted</i>)	H354600-3300-270-276-0029
10	Overall system. (Overview guidewords apply)	All above

2.2 HAZOP Objective

The objective of this study was to perform a hazard and operability (HAZOP) study. The principal objectives were to:

- Systematically examine the proposed systems and equipment in order to identify the potential hazards to people, plant assets, operations and the environment.
- Assess the hazards and the proposed methods of control and decide on appropriate actions which will enable the risks to be reduced or eliminated.

- Assess the design and operations controls and their effects on the potential hazards.
- Document the proposed actions and assign people to be responsible for completing each action and dates for completion
- Get engagement and alignment from the stakeholders around the key hazards and recommended controls.

2.3 HAZOP Methodology

A HAZOP is a detailed systematic examination of a process and/or design. It aims to identify and assess the potential hazards and operational problems and the proposed methods of their control. It is undertaken by a group comprised of the design, operations and maintenance personnel who are familiar with the process. Where hazards or potential operational problems are identified, appropriate changes to the design or procedures are recommended.

The HAZOP procedure is facilitated by a comprehensive checklist of guidewords, which prompt the team to think of potential problems. Three types of guidewords were used in this study:

- Fluid systems guidewords; which are appropriate for examination of logical operational units at the detail level. It was determined during the study that the following guidewords were not required in this workshop:
 - ♦ Agitation, Rotation, Speed
 - ♦ Volume Mass
 - ♦ Tension, Current, Frequency Power
- Non-fluid systems guidewords; which are appropriate for examination of physical processing equipment such as conveyors and stockpile machines. It was agreed that there were no cases where these words were to be applied in this study.
- Overview guidewords; used in reviewing the system holistically, including the interface with the environment.

A list of the HAZOP guidewords used in this study is given in Table 2-2.

Table 2-2: HAZOP Guidewords

Fluid System	Non Fluid Guidewords	Overview
High Flow – High Level	Position	Toxicity
Low Flow - Low Level	Movement	Physical Damage
Reverse Flow	Load	Fire/Explosion
High Pressure	Energy	Environment impact
Low Pressure	Timing	Materials of construction

Fluid System	Non Fluid Guidewords	Overview
High Temperature	Contamination	Access
Low Temperature	Size	Utilities and services
Process Control	Process Control	Start up / Shut down
Contamination	Maintenance	Safety Equipment
Electrical Safety		Natural Hazards
Maintenance		Inspection & Testing
Agitation, Rotation, Speed		Procedures Development & Documentation
Volume, Mass		Quality Control
Tension, Current, Frequency, Power		

The HAZOP is carried out by a team including the design, operations and maintenance people who are familiar with the plant and relevant Vendors and management. The technique assumes that errors in the design arise because of the complexity. To cope with this HAZOP uses a systematic examination to identify where deviations from the design intent can occur.

HAZOP meetings are chaired by a facilitator who has an adequate knowledge of the system being assessed, and also has good experience in the HAZOP technique. The role of the facilitator is to facilitate and coordinate the compilation of issues based on available information and the perceptions of the workshop team. The level of detail and time involved in the study precludes the facilitator from validating the identified issues, or determining whether they had been underrated, overlooked or misinterpreted. The facilitator recorded the outcomes of the discussions in an electronic worksheet using PHA Pro software. These records were displayed on the screen to ensure they communicated the consensus outcomes.

It was initially planned to assign risk levels for risks before and after the application of recommended controls. The risk matrix proposed for this was from PRNC HAZOP Record PR-E-235E_HazOp_Rev8. However, it was felt that the rating of the risks could be left for another occasion, if it is required at all.

3. HAZOP Participants

Personnel from PRNC and Hatch attended the HAZOP. The participants are shown in Table 3-1.

Table 3-1: HAZOP Participants

Name	Responsibility	Company
Jeremy Szopa	Project Manager	PRNC
Phillipe Prevot	Project Director	PRNC
Mauricio Orsolani	Supervisor Operation DWP1	PRNC
Lionel Aune	Maintenance Planner	PRNC
Thomas Lundqvist	Construction Supervisor	PRNC
Andre Rosa		PRNC
Claire Vaguener	Geotechnical Engineer	PRNC
Werner Gerritsen	Engineering Manager	Hatch
Pascal Pouliot	Area Manager	Hatch
Ian Weatherhead	Design Coordinator	Hatch
Brett Stewart	Mechanical Lead	Hatch
Nicholas Henderson	Structural Lead	Hatch
Cledson Sabino	Electrical and Control Lead	Hatch
David Martin	Civil	Hatch
Flore Blanchet	Process Lead	Hatch
Duncan Faulkner	Process	Hatch
Winnie Chan	Tailings	Hatch
Alan Cooper	Project Controls	Hatch
Bruno Dallacqua	Electrical Designer	Hatch
Glenn Howarth	Piping Designer	Hatch
Sylvain Bourque	Project Advisor	Hatch
John Yesberg	Facilitator	Hatch

4. Recommendations

In the table of recommendations, the Causes column is a reference to the node, deviation (guideword), and cause, as listed in Appendix B. For example, cause 2.11.1 refers to Node 2, Deviation 11, Cause 1.

Recommendation	Causes	Action By
1. Ensure appropriate pump control in place.	Causes: 1.1.1	Flore
2. Calculate condition-based maintenance for sprinklers. Baseline pressure/flow characteristics during commissioning and look for anomalies during operation.	Causes: 1.2.1	Flore
3. Check whether screen overflow will be directed to bund or bin.	Causes: 1.2.1	Brett
4. Consider whether limit switches are required on manual valves to interlock pump start.	Causes: 1.2.1	Brett
5. Confirm pump stops on insufficient flow after 30 seconds.	Causes: 1.2.1	Mateus
6. Need to ensure consistent overall approach to control of dilution (internal and external)	Causes: 1.8.1	Brett
7. Review possibility of blockage of this node (and also existing KO2 line) and flush methods.	Causes: 2.11.1	Brett
8. Standard operating procedure should avoid closing the valve when line is full of slurry - should clean/flush first.	Causes: 2.11.1	PRNC
9. Review dead legs as part of design review, and consider flushing capability for gate valves.	Causes: 2.11.1	Parking Lot
10. Show vacuum breakers on P&ID	Causes: 3.1.1	Brett
11. Confirm thickener underflow pumps can handle this level of solids.	Causes: 3.2.3	Brett
12. Verify that KO2 barge pump can provide sufficient flow for flushing.	Causes: 3.2.2	Brett
13. Review of next P&ID version to identify flushing configurations	Causes: 3.2.2	Brett
14. Confirm that control strategy is adequate to cope with capacity. Will require changes to existing assets.	Causes: 5.1.1	Brett
15. Identify strategy for dealing with excess water in KO2 area.	Causes: 5.1.2	Brett
16. Confirm that pipeline can handle sufficient pressure and pumping arrangement. Consider removing vent. May require pressure measurement (Antenna Pass modifications).	Causes: 5.1.3	Brett
17. Ensure temperature transmitters are shown at pump discharges and thickener overflow and barge discharge as required.	Causes: 5.6.1	Mateus
18. Ensure that automatic valves are used to select destination. (Currently in markups)	Causes: 5.6.1	Mateus

Recommendation	Causes	Action By
19. Ensure functional description integrates existing and new systems well (noting separate DCS, the two DCS systems do not communicate). 285 will need to control the water that goes to 285. 285 will need information about what is coming from DWP2 - not necessarily with a DCS interface.	Causes: 5.8.1	Mateus, Flore
20. Ensure pump 36/37 start is interlocked to control valve.	Causes: 7.1.2	Mateus
21. Add flow switch on common discharge to protect pump.	Causes: 7.2.1	Mateus
22. Add spool for basket strainer at suction of pumps 012, 013.	Causes: 7.9.1	Brett
23. Verify P&ID updated correctly.	Causes: 8.2.2	Brett
24. Check valve to be removed upstream of accumulator	Causes: 8.4.1	Brett
25. Ensure we purchase a oil/water separator for the condensate system (already specified.)	Causes: 8.9.1	Brett
26. Once equipment has been purchased, ensure that condensate from dryer and accumulator are routed to compressor.	Causes: 8.9.1	Brett
27. Clarify with vendor(s) whether bypass is available.	Causes: 8.11.2	Brett
28. Incorporate point for external compressed air source	Causes: 8.11.3	Brett
29. Verify that external source pressure is not too high, else include pressure control valve.	Causes: 8.11.3	Brett
30. Confirm pressure requirement for instrument and service air	Causes: 8.11.3	PRNC
31. Ensure that fire detection is in place	Causes: 10.3.1	Brett
32. Confirm P&ID revision shows that valves going to thickener will fail closed on loss of power, and valves to KO2 will fail open.	Causes: 10.7.1	Mateus
33. Assess the possibility of water hammer as valves operate on electrical failure.	Causes: 10.7.1	Brett
34. Confirm that valves fail correctly, and that suitable services (e.g. accumulator) are included.	Causes: 10.7.1	Brett
35. Consider supplying emergency power to thickener area air compressor.	Causes: 10.8.1	Cledson
36. Ensure that thickener underflow pump has emergency power.	Causes: 10.8.1	Cledson
37. Revisit load shedding plan - this area may no longer be a priority for power. To be determined.	Causes: 10.9.1	PRNC

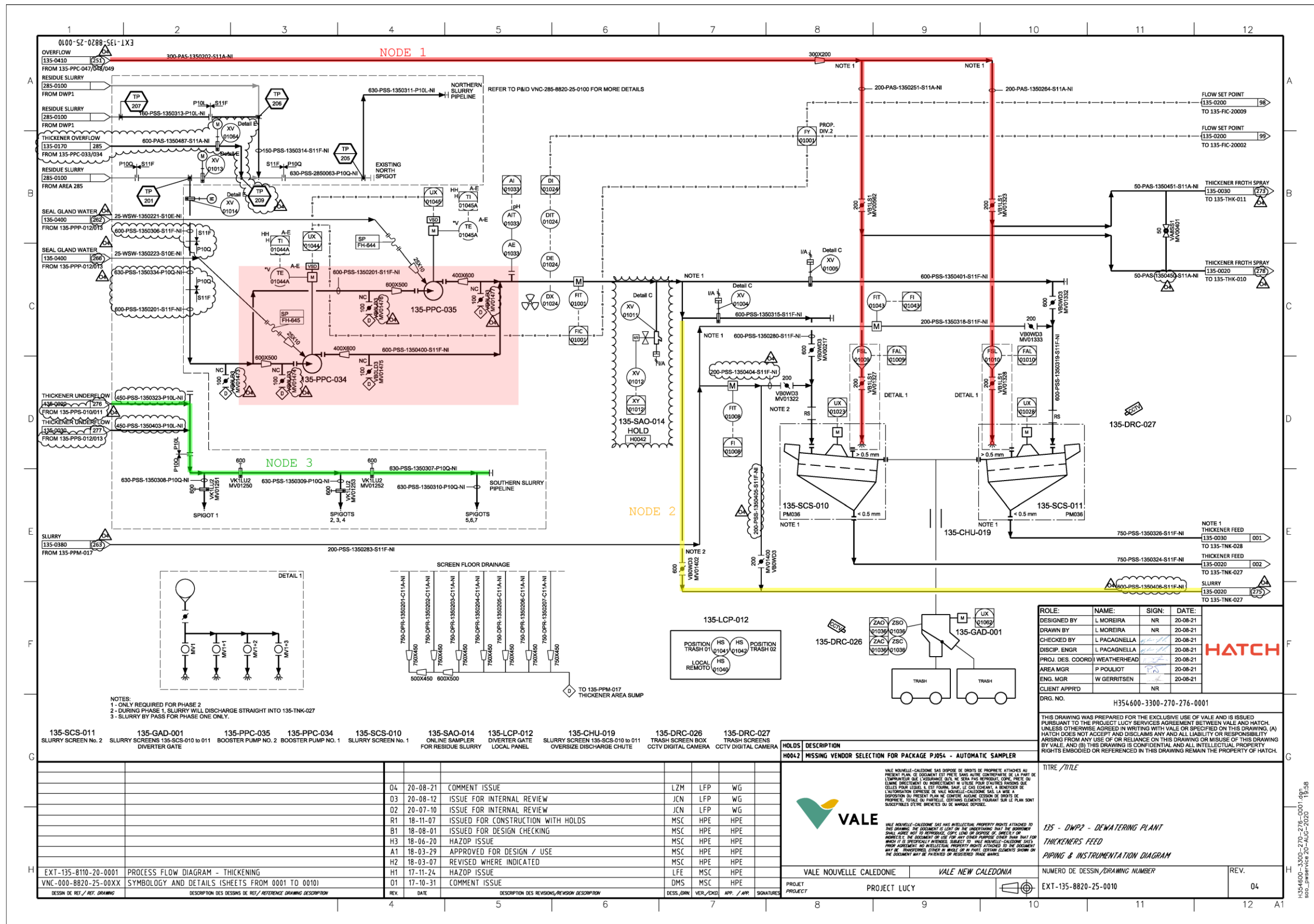
5. References

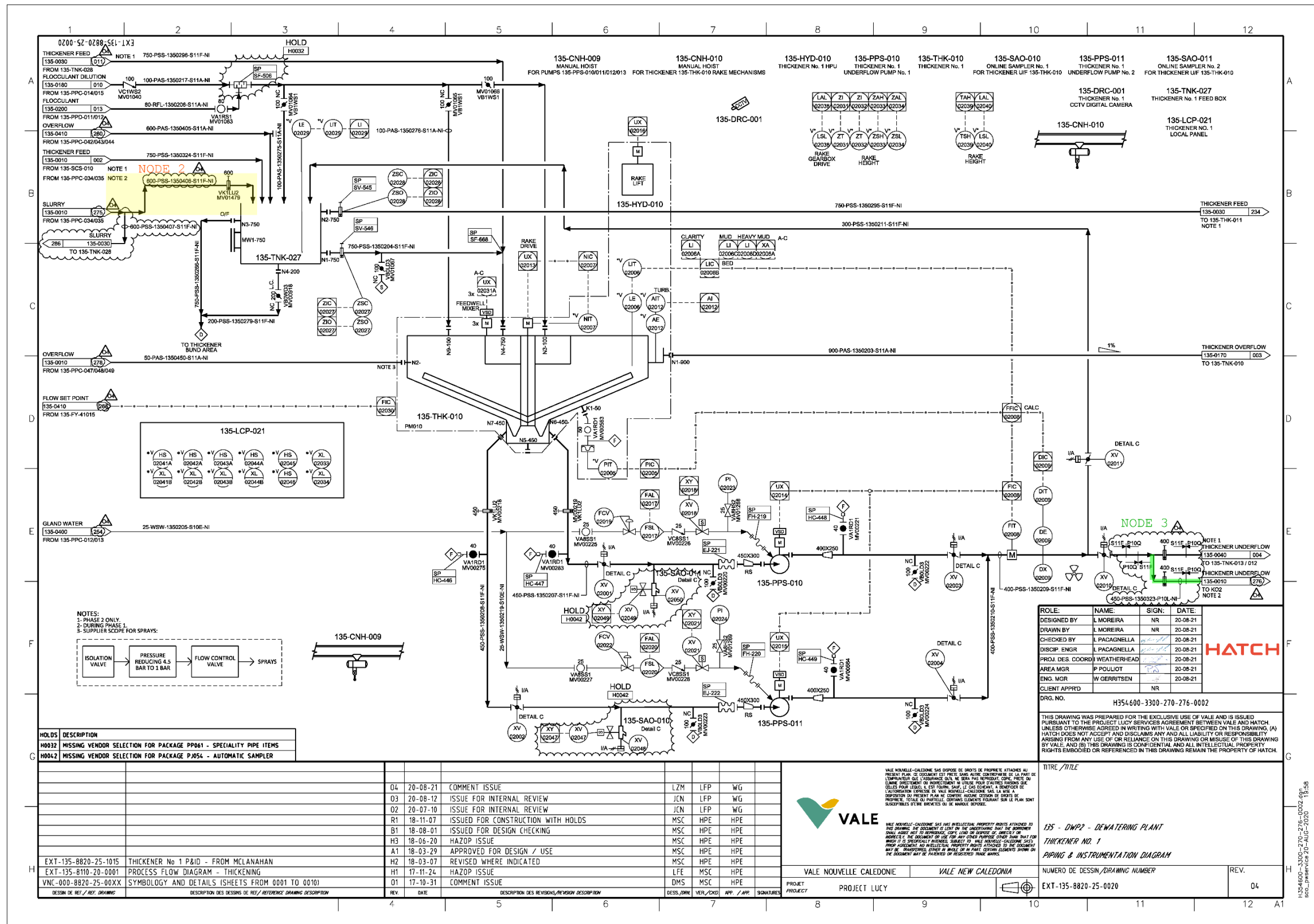
The following drawings were used for the HAZOP.

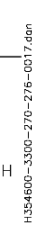
Title	Drawing Number	Hatch Drawing Number	Rev	Date
Thickening PFD	EXT-135-8110-20-0001	H354600-0000-210-282-0001	A5	2020-08-14
Thickeners Feed P&ID	EXT-135-8820-25-0010	H354600-3300-270-276-0001	04	2020-08-21
Thickener No. 1 P&ID	EXT-135-8820-25-0020	H354600-3300-270-276-0002	04	2020-08-21
Thickener No. 2 P&ID	EXT-135-8820-25-0030	H354600-3300-270-276-0003	04	2020-08-21
Thickener Overflow Tanks P&ID	EXT-135-8820-25-0170	H354600-3300-270-276-0017	04	2020-08-21
Thickener Overflow Tanks P&ID	EXT-135-8820-25-0170	H354600-3300-270-276-0017	R1	2018-11-07
Flocculant Plant and Distribution P&ID	EXT-135-8820-25-0200	H354600-3300-270-276-0020	04	2020-08-21
Fire Water Ring Main	EXT-135-8820-25-0290	H354600-3300-270-276-0029	04	2020-08-21
Squeezing Air / Service Compressors P&ID	EXT-135-8820-25-0330	H354600-3300-270-276-0033	04	2020-08-21
Thickener Process Water Tank P&ID	EXT-135-8820-25-0400	H354600-3300-270-276-0040	03	2020-08-21
Screen Spray Water Pumps and Overflow Dilution Pumps P&ID	EXT-135-8820-25-0410	H354600-3300-270-276-0041	03	2020-08-21

Appendix A

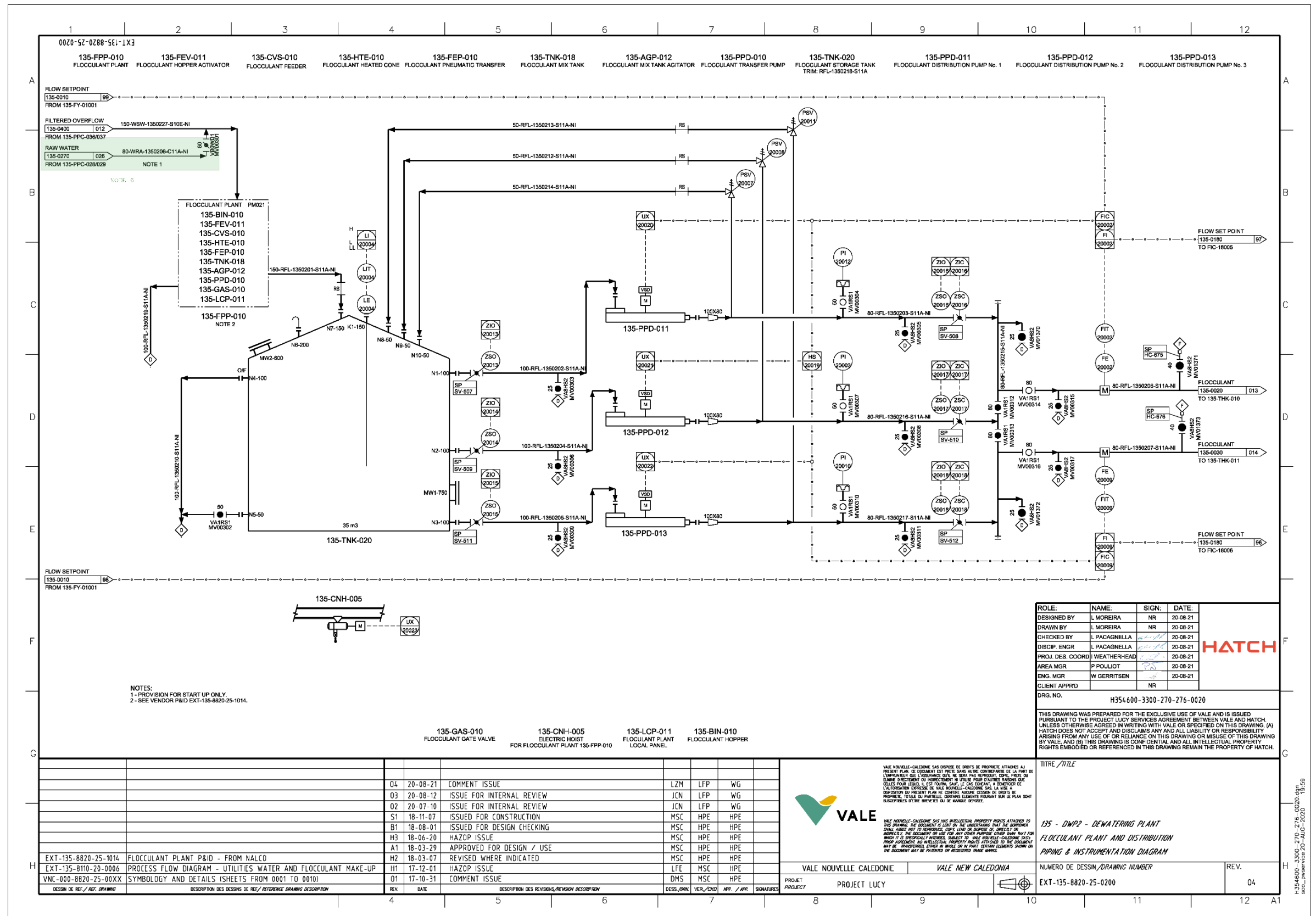
Marked up Nodes (P&ID)

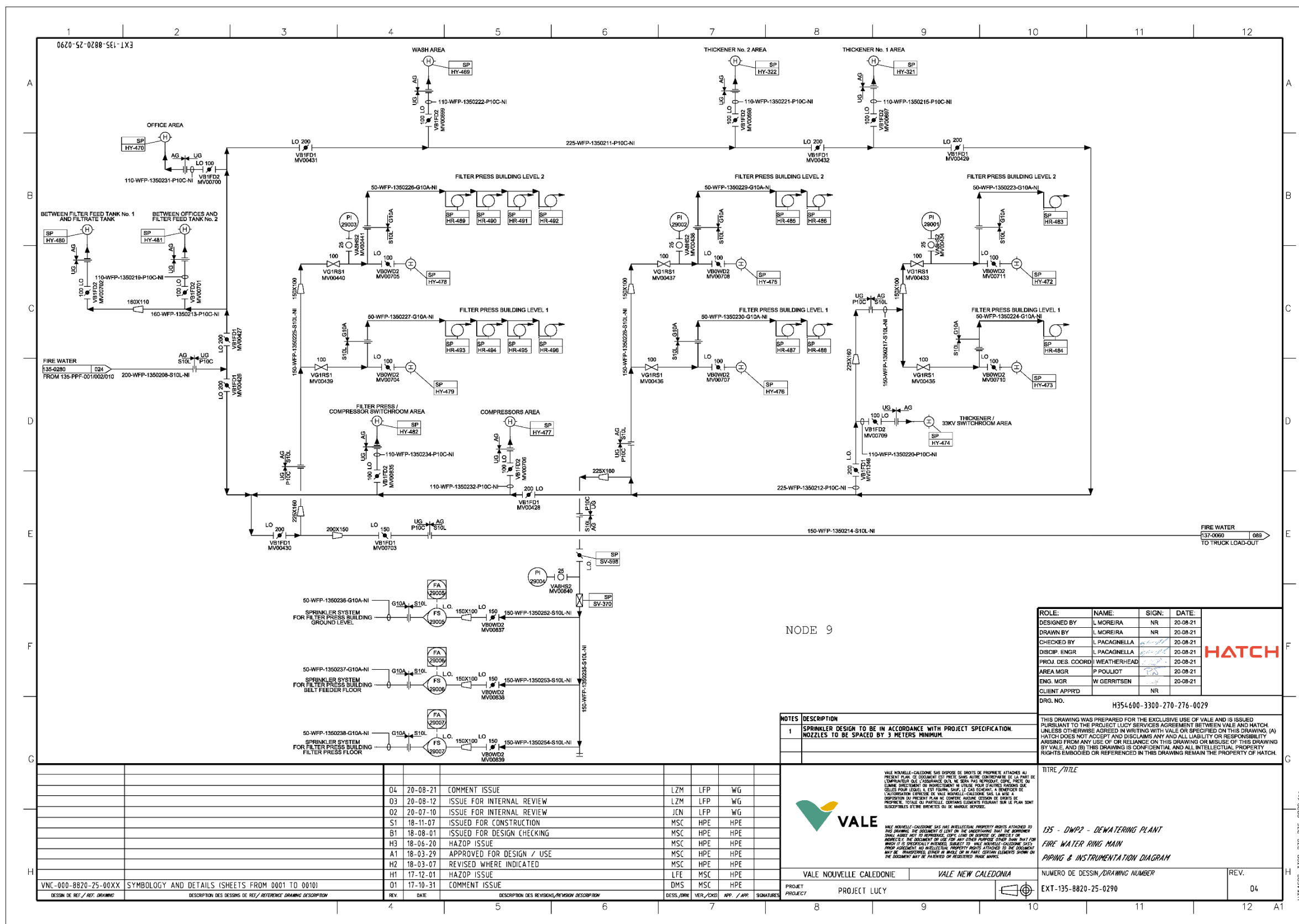


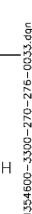




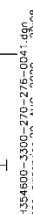












Appendix B

Mini-HAZOP Study Worksheet

Node	Deviation	Cause	Consequence	Effective Safeguards	Recommendations	Responsibility
1. Thickener overflow to screen spray wash	1. High Flow – High Level	1. 3 pumps running instead of 2	1. Excess fluid to screens, extra dilution		1. Ensure appropriate pump control in place.	Flore
	2. Low Flow - Low Level	1. Not enough water	1. Blocked screen, possible overflow	1. Low flow switch/alarm	2. Calculate condition-based maintenance for sprinklers. Baseline pressure/flow characteristics during commissioning and look for anomalies during operation.	Flore
			2. Damage to pumps	2. flow meter after pumps	3. Check whether screen overflow will be directed to bund or bin.	Brett
				3. Pressure transmitter after pumps	4. Consider whether limit switches are required on manual valves to interlock pump start.	Brett
				4. Pump current measurement & control, tank level above NPSH requirement.	5. Confirm pump stops on insufficient flow after 30 seconds.	Mateus
				5. CCTV		
		2. Problem with pumps				
		3. Closed suction valve (manual) (similar to not enough water)				
		4. Sprinklers blocked from solids contamination				
	3. Reverse Flow	1. Liquid will flow backwards if pumps stop.	1. Damage to pump	1. NRV has been marked up on discharge of each pump.		
				2. Automatic valves on each pump discharge. No water hammer expected.		
	4. High Pressure	1. Same as Low Flow.		1. Pipe is specified to cover max pressure from pumps.		
				2. Pump casing pressure needs to be rated above pump dead-head pressure.		
	5. Low Pressure	1. Same as Low Flow.				
		2. Leak on pump discharge	1. Low flow to screens	1. Flow meters & flow switches		
			2. Spillage into bunded area	2. Bund		
		3. Pump failure	1. Same as discussed under Low Flow	3. Pipe rated sufficiently		
				1. Redundant pumps		
	6. High Temperature	1. No foreseeable cause		1. Pump dead head will trip pump.		
	7. Low Temperature	1. No foreseeable cause				
	8. Process Control	1.		1. Pumps are fixed speed.	6. Need to ensure consistent overall approach to control of dilution (internal and external)	Brett
	9. Contamination	1. Contamination can block spray	1. Same as discussed under Low Flow	1. Materials of construction ok (stainless)		
	10. Electrical Safety	1. No specific causes related to this node				
	11. Maintenance	1. Automatic valve fails open	1. May be difficult to maintain pump	1. Valve is currently specified as "fail last".		
	12. Agitation, Rotation, Speed	1. No foreseeable cause				
	13. Volume, Mass	1. Not applicable				
	14. Tension, Current, Frequency, Power	1. Not specific to this node				
2. Screen bypass to thickener feed boxes	1. High Flow – High Level	1. Overflow thickener feed boxes. (Phase 1 has only one thickener operating.)	1. Loss of material	1. Overflow directed to bund		
				2. One thickener can take full flow		
	2. Low Flow - Low Level	1. Possible if low flow from Area 285	1. No problems identified.			
	3. Reverse Flow	1. No foreseeable cause				
	4. High Pressure	1. Blocked line or gate valve closed.	1. Low flow, potential damage to pumps in Area 285.	1. Pressure gauge and flow meter in Area 285.		
				2. Valves only need to be operated in major configuration changes.		
				3. Valve is lockable.		

Node	Deviation	Cause	Consequence	Effective Safeguards	Recommendations	Responsibility
	5. Low Pressure	1. Leak or feed pumps not operating	1. Same as low flow			
	6. High Temperature	1. No foreseeable cause				
	7. Low Temperature	1. No foreseeable cause				
	8. Process Control	1.		1. This is a manual operation - there is no control.		
	9. Contamination	1. Little rocks/sand/gypsum may reach thickener		1. Reason for bypass: limited power available at the beginning. Screens are primarily to protect filters. Since thickened slurry goes to KO2, screens are not essential. Screen wash pumps use significant power. Gives flexibility to operate without filters.		
	10. Electrical Safety	1. Not specific to this node				
	11. Maintenance	1. Could the line be blocked due to slurry solids settling, especially if a valve is left closed for a long time (especially in phase 2)		1. Flush line using the same procedure as Area 285 lines. 2. Difficult to block a 600mm line. 3. Already a connection from KO2 line at Antenna Pass.	7. Review possibility of blockage of this node (and also existing KO2 line) and flush methods. 8. Standard operating procedure should avoid closing the valve when line is full of slurry - should clean/flush first. 9. Review dead legs as part of design review, and consider flushing capability for gate valves.	Brett PRNC Parking Lot
3. Thickener underflow to southern slurry pipeline tie-in	1. High Flow – High Level	1. Siphon		1. There are vacuum breakers in the line	10. Show vacuum breakers on P&ID	Brett
	2. Low Flow - Low Level	1. Pump failure. All these causes are similar to Lucy 1.0 - only difference now is that there are two destinations.		1. Flow and pressure transmitters		
		2. Blocked line		1. P&IDs do not currently show all flush points, but they have been added.	12. Verify that KO2 barge pump can provide sufficient flow for flushing. 13. Review of next P&ID version to identify flushing configurations	Brett Brett
		3. Slurry too thick		1. Maximum solids% is 42-45	11. Confirm thickener underflow pumps can handle this level of solids.	Brett
		4. Thickener cone blocked		1. Covered in previous hazop - flush points on thickener cone.		
	3. Reverse Flow	1. No foreseeable cause				
	4. High Pressure	1. Same as Low Flow.				
		2. What if all valves are closed	1. Dead head pump	1. Flow measurement - Pump will trip		
	5. Low Pressure	1. Leak	1. Not entirely in banded area, but in the pipeline corridor	1. Same risk as current situation. 2. Flow transmitter will make this apparent		
		2. Pump failure	1. Same as discussed under Low Flow			
	6. High Temperature	1. No foreseeable cause				
	7. Low Temperature	1. No foreseeable cause				
	8. Process Control	1. No foreseeable cause				
	9. Contamination	1. No foreseeable cause				
	10. Electrical Safety	1. No specific causes related to this node				
	11. Maintenance	1. Same as Low Flow.				
4. Removal of runoff water line to thickener overflow tanks	1. High Flow – High Level					
	2. Low Flow - Low Level					
	3. Reverse Flow					
	4. High Pressure					
	5. Low Pressure					
	6. High Temperature					
	7. Low Temperature					

Node	Deviation	Cause	Consequence	Effective Safeguards	Recommendations	Responsibility
	8. Process Control					
	9. Contamination					
	10. Electrical Safety					
	11. Maintenance					
5. Thickener overflow to KO2	1. High Flow – High Level	1. Total flow to 285 is limited.		1. Reason for this node: to enhance temperature control of fluid going to 285, we can divert some overflow to KO2 if required.	14. Confirm that control strategy is adequate to cope with capacity. Will require changes to existing assets.	Brett
				2. Water balance shows no KO2 overflow.		
		2. Weather event may increase flow to KO2	1. Overflow KO2		15. Identify strategy for dealing with excess water in KO2 area.	Brett
		3. Flow may be too high for gravity to empty line from Antenna Pass.	1. Slurry may come out vent at Antenna Pass		16. Confirm that pipeline can handle sufficient pressure and pumping arrangement. Consider removing vent. May require pressure measurement (Antenna Pass modifications).	Brett
		4. Temperature control may lead to too much flow to KO2.		1. Calculations indicate that this will not be a problem when operating in design parameters. Not foreseeable.		
	2. Low Flow - Low Level	1. Pump failure, blocked valve, etc.	1. No problems identified.			
			2. Extra capacity in KO2			
	3. Reverse Flow	1. New tie in may allow for reverse flow		1. Existing pressure balance and NRVs have been designed to prevent this.		
	4. High Pressure	1. Valve misconfiguration	1. Pump failure	1. Flow monitoring on all pumps		
	5. Low Pressure	1. Same as Low Flow.				
	6. High Temperature	1.			17. Ensure temperature transmitters are shown at pump discharges and thickener overflow and barge discharge as required.	Mateus
					18. Ensure that automatic valves are used to select destination. (Currently in markups)	Mateus
	7. Low Temperature	1. No foreseeable cause	1. Happy.			
	8. Process Control	1. Same as for High Temperature.			19. Ensure functional description integrates existing and new systems well (noting separate DCS, the two DCS systems do not communicate). 285 will need to control the water that goes to 285. 285 will need information about what is coming from DWP2 - not necessarily with a DCS interface.	Mateus, Flore
	9. Contamination	1. No foreseeable cause				
	10. Electrical Safety	1. No specific causes related to this node				
	11. Maintenance					
6. Flocculant make-up water source	1. High Flow – High Level	1. Loss of control on pump	1. Over dilution, bad flocculant batch	1. Flow is controlled.		
	2. Low Flow - Low Level	1. Pump failure	1. High concentration of flocculant - lumps.	1. Batch process - don't use the batch if it is bad.		
				2. The change from overflow water to raw water reduces the chance of solids.		
	3. Reverse Flow	1. Pump failure	1. Damage to pump	1. NRV installed.		
	4. High Pressure	1. Overpressure - closed valves	1. Pipe rupture	1. Pipe rated sufficiently		
	5. Low Pressure	1. Pump failure	1. Same as discussed under Low Flow			
	6. High Temperature					
	7. Low Temperature					
	8. Process Control	1.		1. Batch process. Same as previous hazop.		
	9. Contamination	1.		1. Reduced by using raw water.		
	10. Electrical Safety					
	11. Maintenance					

Node	Deviation	Cause	Consequence	Effective Safeguards	Recommendations	Responsibility
7. Thickener process water tank	1. High Flow – High Level	1. Failure to control incoming water	1. Overflow	1. Overflows to concrete pad, then to bund	20. Ensure pump 36/37 start is interlocked to control valve.	Mateus
		2. Gland water pumps over pumping	1. No problems identified.	1. Recirculation line		
				2. Control pressure & flow for gland water		
	2. Low Flow - Low Level	1. Suction valve closed, pump has no water.	1. Burn mechanical seal	1. Gland water flow switches will protect pumps.	21. Add flow switch on common discharge to protect pump.	Mateus
			2. Insufficient gland water			
	3. Reverse Flow					
	4. High Pressure	1. Same as for High Flow				
	5. Low Pressure	1. Same as for Low Flow				
	6. High Temperature					
	7. Low Temperature					
	8. Process Control					
	9. Contamination	1. Algae in tank	1. Block pumps		22. Add spool for basket strainer at suction of pumps 012, 013.	Brett
8. Thickener air compressor	10. Electrical Safety					
	11. Maintenance					
	1. High Flow – High Level					
	2. Low Flow - Low Level	1. Compressor failure	1. Lack of instrument air	1. Pressure instrumentation	23. Verify P&ID updated correctly.	Brett
		2. Service air comes directly from compressor	1. Compressor always running	1. P&ID has been marked up. Service air now comes from accumulator.		
	3. Reverse Flow					
	4. High Pressure	1. Compressor may not shut off	1. Overpressure in accumulator	1. Relief valve in place	24. Check valve to be removed upstream of accumulator	Brett
	5. Low Pressure	1. Compressor failure	1. As for low flow			
	6. High Temperature	1. High temperature air from compressor		1. Accumulator will lower temperature.		
				2. Compressor has thermal cutout.		
	7. Low Temperature					
	8. Process Control					
	9. Contamination	1. Possibility of oil in condensate		1. Automatic alarms when oil is full.	25. Ensure we purchase a oil/water separator for the condensate system (already specified.)	Brett
					26. Once equipment has been purchased, ensure that condensate from dryer and accumulator are routed to compressor.	Brett
	10. Electrical Safety					
	11. Maintenance	1. Outdoor equipment may deteriorate		1. System has been specified for outdoor location.		
		2. May need to bypass dryer		1. System is a single vendor package	27. Clarify with vendor(s) whether bypass is available.	Brett
		3. Compressor failure			28. Incorporate point for external compressed air source	Brett
9. Fire water					29. Verify that external source pressure is not too high, else include pressure control valve.	Brett
					30. Confirm pressure requirement for instrument and service air	PRNC
10. Overall system	1. Toxicity	1. Slurry may not be adequately neutralized	1. This is normal operation.	1. pH control on the line entering the thickeners		
	2. Physical Damage	1. No new causes foreseeable.		2. Safety showers in place		
				1. Plant is located to avoid interactions with DWP1 activities		
				2. Design minimizes possibilities of pipe damage due to traffic at road crossings		

Node	Deviation	Cause	Consequence	Effective Safeguards	Recommendations	Responsibility
				3. Mobile equipment moving grits, but layout allows for better movement. Not a new risk.		
	3. Fire/Explosion	1. Screens - hydraulic units, screen deck is polyurethane - static electricity		1. Hydraulic unit should have temperature sensors. 2. Previous requirement for fire/smoke detection	31. Ensure that fire detection is in place	Brett
		2. Hot work causes spark on polyurethane		1. Permit & administrative controls require separate controls.		
	4. Environment impact	1. Tank leaks, overflows		1. Contained by bund		
				2. Piping corridor risk is not increased.		
	5. Materials of construction	1. Corrosion		1. Using existing materials - stainless or HDPE.		
	6. Access	1.		1. Access is improved over the previous DWP2 design.		
	7. Utilities and services	1. Loss of electricity	1. Bypass thickeners and go to KO2	1. None required. Automated (motorized) valves.	32. Confirm P&ID revision shows that valves going to thickener will fail closed on loss of power, and valves to KO2 will fail open.	Mateus
					33. Assess the possibility of water hammer as valves operate on electrical failure.	Brett
					34. Confirm that valves fail correctly, and that suitable services (e.g. accumulator) are included.	Brett
	8. Start up / Shut down	1.		1. Already captured requirement to flush lines that may contain solids	35. Consider supplying emergency power to thickener area air compressor.	Cledson
				2. Can operate with or without screens	36. Ensure that thickener underflow pump has emergency power.	Cledson
				3. Backup generator to supply filter feed tank agitators, flocculant tanks, and filter rakes (part of design for Lucy 1.0)		
	9. Safety Equipment	1. Electrical overload			37. Revisit load shedding plan - this area may no longer be a priority for power. To be determined.	PRNC
		2. No new causes foreseeable.				
	10. Natural Hazards	1. Heavy rain, cyclone (move to Environmental guideword)	1. Thickeners, bunds overflow, potential environmental discharge.	1. Contact water on the hill or the pad takes water by gravity drain (open culvert) to KO2.		
	11. Inspection & Testing	1. No new causes foreseeable.				
	12. Procedures Development & Documentation					
	13. Quality Control					